

# Selective Conversion of CO<sub>2</sub> to CO with High Efficiency Using an Inexpensive Bismuth-Based Electrocatalyst

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## **Supporting Information**

ABSTRACT: The wide-scale implementation of solar and other renewable sources of electricity requires improved means for energy storage. An intriguing strategy in this regard is the reduction of  $CO_2$  to CO, which generates an energy-rich commodity chemical that can be coupled to liquid fuel production. In this work, we report an inexpensive bismuth-carbon monoxide evolving catalyst (Bi-CMEC) that can be formed upon cathodic polarization of an inert glassy carbon electrode in acidic solutions containing Bi<sup>3+</sup> ions. This catalyst can be used in conjunction with ionic liquids to effect the electrocatalytic conversion of CO<sub>2</sub> to CO with appreciable current density at overpotentials below 0.2 V. Bi-CMEC is selective for production of CO, operating with a Faradaic efficiency of approximately 95%. When taken together, these correspond to a high-energy efficiency for CO production, on par with that which has historically only been observed using expensive silver and gold cathodes.

**S** torage of solar and other sources of renewable electricity may be enabled by the catalytic production of fuels such as  $H_2$  or reduced carbon-containing compounds via the electrochemical reduction of  $H_2O$  or  $CO_2$ , respectively. The renewable production of reduced carbon compounds is especially attractive,<sup>1</sup> as liquid fuels can directly address energy needs associated with transportation,<sup>2</sup> which account for nearly 30% of the U.S. energy demand.<sup>3</sup> An attractive strategy for the synthesis of carbon-based fuels is the marriage of a robust electrocatalyst for  $CO_2$  reduction with a photoelectrochemical device or a conventional electrolyzer powered by a renewable source of electrical current. One such energy-storing process is the  $2e^{-}/2H^+$  reduction of  $CO_2$  to CO (Eq 1),

$$\mathrm{CO}_2 + 2\mathrm{H}^+ + 2\mathrm{e}^- \to \mathrm{CO} + \mathrm{H}_2\mathrm{O} \tag{1}$$

which produces an energy-rich commodity chemical. CO can be reacted with  $H_2O$  via the water–gas shift to generate  $H_{2\nu}$  and this CO/H<sub>2</sub> mixture (syngas) can be used to generate synthetic petroleum and liquid fuels using Fischer–Tropsch methods<sup>4–6</sup> for direct integration into energy storage and distribution networks.<sup>7</sup>

Much effort has been devoted to the heterogeneous reduction of  $CO_2$  at metallic electrodes, with the goal of driving selective formation of CO via Eq 1. A number of cathode materials can facilitate this reaction; however, only noble metals such as Ag and Au can catalyze this reaction with Faradaic efficiencies (FEs) that are in excess of 80% at ambient

pressures.<sup>8</sup> The use of noble metal cathodes for production of CO has been hampered by the exorbitant cost of these materials, which eliminates their practical use on the scale required for alternative fuel synthesis. Indeed, the dearth of cost-effective systems that can efficiently and selectively drive Eq 1 highlights the need for new electrode/catholyte pairings that can selectively promote the electrocatalytic conversion of CO<sub>2</sub> to CO at appreciable rate (high current density) and low overpotential.

Bismuth is an attractive material for development of heterogeneous CO<sub>2</sub> reduction catalysts, as this metal is nontoxic and has a very small environmental impact. Moreover, Bi is a byproduct of Pb, Cu, and Sn refining, and has few significant commercial applications, resulting in the price of Bi being low and stable. Despite these attractive qualities, there has been only one report of electrocatalytic CO2 reduction using Bi,<sup>9</sup> and the ability of this metal to drive CO production has not been demonstrated. As such, development of Bi-based cathodes for conversion of CO<sub>2</sub> to CO would represent an important development for the fields of CO<sub>2</sub> electrocatalysis and renewable energy conversion. To this end, we electrodeposited a Bi-containing material onto an inert electrode substrate; reduction of an aqueous solution of 20 mM Bi(NO<sub>3</sub>)<sub>3</sub> containing 0.5 M KBr and 1.0 M HCl using a glassy carbon electrode (GCE) produces the CV trace shown in Figure 1A, which is characterized by a broad cathodic wave. Controlled potential electrolysis (CPE) was carried out at -0.21 V versus the saturated calomel electrode (SCE; all potentials are referenced to this electrode) for quiescent acidic Bi<sup>3+</sup> solutions until ~3 C/cm<sup>2</sup> had been passed, leading to electrodeposition of a gray, nonlustrous material on the GCE surface. Glassy carbon was used as the working electrode to



Figure 1. (a) Cyclic voltammogram in 1.0 M HCl (aq) and 0.5 M KBr (aq) containing 20 mM  $Bi^{3+}$ . (b) SEM image of a Bi-modified GCE.

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**Figure 2.** (a) CV traces recorded for Bi-modified and bare GCEs in MeCN containing 20 mM [EMIM]BF<sub>4</sub>. Inset: Bi-modified GCE in MeCN without IL. (b) Total current density  $(j_{tot})$  profiles for Bi-CMEC and GCE at -1.95 V in MeCN. (c) Total current density  $(j_{tot})$  Tafel plot for Bi-CMEC with 20 mM [BMIM]PF<sub>6</sub> in MeCN. All electrochemistry was performed using 0.1 M TBAPF<sub>6</sub> as electrolyte.

ensure that the base substrate supported negligible background activity for CO<sub>2</sub> reduction.

The morphology of the deposited material was examined by scanning electron microscopy (SEM). As shown in Figure 1B, the electrode is coated by an array of striated clusters, interspersed within a film of smaller crystallites. Magnification of the micrometer-sized clusters shows that the basic morphology of this material is reminiscent of a flower or rosebud. Energy-dispersive X-ray (EDX) analysis was performed on 40  $\times$  40  $\mu$ m<sup>2</sup> regions of several independently prepared samples of the electrodeposited material (Figure S1). The surface of the material was also analyzed by X-ray photoelectron spectroscopy (XPS). All elements detected by EDX are also accounted for by XPS (Figure S2), which identifies Bi, Cl, and Br as the principal elemental components in a ratio of roughly 7:1:1 with trace amounts of O and K also present. High-resolution XPS spectra for the bismuth region reveal Bi 4f<sub>7/2</sub> signals at 156.5 and 159.3 eV, which are in the range typical of Bi<sup>0</sup> and Bi<sup>3+</sup> (Figure S2B) and integrate to a ratio of  $\sim$ 2:1. When taken together, the EDX and XPS analyses indicate that reduction of acidic solutions of Bi3+ containing KBr leads to deposition of a microcrystalline material containing metallic Bi<sup>0</sup> and Bi<sup>3+</sup> ions that has incorporated a significant amount of chloride and bromide along with traces of oxygen and potassium. The presence of oxygen and halide atoms in the electrodeposited material balances the charge of the Bi<sup>3+</sup> ions.

The ability of the Bi-modified electrode to electrochemically activate  $CO_2$  was assessed in MeCN, which supports a large electrochemical window and is commonly employed for  $CO_2$  electrocatalysis. As shown in the inset of Figure 2A, scanning to negative potentials in  $CO_2$ -saturated solutions of MeCN containing 0.1 M TBAPF<sub>6</sub> shows a small current enhancement as compared to the corresponding experiment under N<sub>2</sub>.

1,3-Dialkyl-substituted imidazolium-based ionic liquids (ILs) can strongly interact with CO<sub>2</sub> and have found application for carbon sequestration.<sup>10,11</sup> Moreover, the ability of such ILs to bind reduced CO<sub>2</sub> intermediates at Ag electrodes and mediate electrochemical generation of CO at low overpotentials has also been demonstrated.<sup>12</sup> With these properties in mind, the IL 1-ethyl-3-methylimidazolium tetrafluoroborate ([EMIM]BF<sub>4</sub>) was added to the CO<sub>2</sub>-saturated MeCN solution, resulting in a dramatic change in the resultant I/V curves. In particular, the onset of a large, irreversible cathodic wave at -1.85 V is indicative of an electrocatalytic process (Figure 2A, red trace).

This current response cannot simply be attributed to reduction of [EMIM] at the electrode surface, as polarization curves recorded in the absence of  $CO_2$  did not show a reduction wave (Figure 2A, black trace), suggesting that the observed cathodic feature corresponds directly to  $CO_2$  reduction.

In order to establish that the electrocatalytic response shown in Figure 2A corresponded to conversion of CO<sub>2</sub> to a reduced carbon product, CPE experiments were performed for a CO<sub>2</sub>saturated solution of MeCN containing 20 mM [EMIM]BF<sub>4</sub> using a Bi-modified GCE. After initiating the CPE at -1.95 V, the reaction headspace was periodically analyzed by gas chromatography (GC). This analysis showed CO to be the sole gaseous product formed during the electrolysis experiment. After 60 min, the CPE was discontinued and the amount of CO in the headspace was quantified; the measured CO levels corresponded to a FE of nearly 95% for the  $2e^{-}/2H^{+}$ conversion of CO<sub>2</sub> to CO, with an average partial current density of  $j_{CO} = 3.77 \pm 0.7$  mA/cm<sup>2</sup> (Figure 2B, red trace; Table 1). Repetition of this experiment under N<sub>2</sub> leads to

Table 1. Faradaic Efficiencies (FE<sub>CO</sub>) and Current Densities  $(j_{CO})$  for Electrocatalytic Reduction of CO<sub>2</sub> to CO at an Applied Potential of -1.95 V vs SCE in MeCN

electrode	ionic liquid	$FE_{CO}$ (%)	$j_{\rm CO}~({\rm mA/cm}^2)$
GCE	$[EMIM]BF_4$	trace	< 0.03 <sup>a</sup>
Bi-CMEC	$[EMIM]BF_4$	$93 \pm 7$	$3.77 \pm 0.7$
Bi-CMEC	none	48 ± 13	$0.11 \pm 0.1$
Bi-CMEC	[BMIM]BF <sub>4</sub>	95 ± 6	$5.51 \pm 1.2$
Bi-CMEC	[BMIM]PF <sub>6</sub>	90 ± 9	$4.82 \pm 0.7$
Bi-CMEC	[BMMIM]BF <sub>4</sub>	76 ± 6	$0.67 \pm 0.5$
<sup>a</sup> Total current density.			

negligible current density (Figure 2B, black trace) and no CO production, indicating that the CO formed under an atmosphere of  $CO_2$  is not simply a product of IL or solvent decomposition. Similarly, repeating this experiment under  $CO_2$  but in the absence of [EMIM] results in a nearly 40-fold decrease in current density (Figure 2B, purple trace) and a substantial reduction in FE for CO production (Table 1). Taken together, these control experiments demonstrate that the IL is integral to the observed electrocatalysis, which is distinguished by high current densities for the selective production of CO from  $CO_2$ .

Additional experiments demonstrate that the observed electrocatalysis cannot simply be attributed to homogeneous

 $\rm CO_2$  reduction mediated by the IL. If the observed electrocatalysis were homogeneous in nature, the identity of the working electrode should have minimal impact on the observed chemistry. Unlike those obtained using a Bi-modified electrode, CV traces recorded for 20 mM [EMIM]BF<sub>4</sub> in MeCN under CO<sub>2</sub> with a glassy carbon working electrode showed virtually no current enhancement upon scanning to negative potentials (Figure 2A, green trace). Similarly, CPE of the CO<sub>2</sub>-saturated solution of MeCN containing [EMIM] at -1.95 V using a GCE resulted in negligible charge passed over the course of a 60 min experiment, and no CO production (Figure 2B, green trace; Table 1). Accordingly, the Bi-modified electrode is intimately involved in the electrocatalytic conversion of CO<sub>2</sub> to CO, and represents the first bismuth–carbon monoxide evolving catalyst (Bi-CMEC).

The performance of Bi-CMEC on GCE was also assessed using more viscous ILs in MeCN. Titration of either the BF<sub>4</sub><sup>-</sup> or  $PF_6^-$  salts of 1-butyl-3-methylimidazolium ([BMIM]) into acetonitrile gave rise to polarization curves similar to that observed for [EMIM]BF4 (Figure S3). Similarly, CPE of MeCN solutions containing 0.1 M TBAPF<sub>6</sub> and 20 mM [BMIM]X (X = BF<sub>4</sub> or PF<sub>6</sub>) at -1.95 V led to the rapid production of CO with near-quantitative FEs (Table 1). Notably, the CPEs produced only trace levels of H<sub>2</sub> and no detectable formate, oxalate, or glyoxalate, which are often observed upon electrochemical reduction of CO2 in organic solvents.<sup>13,14</sup> This result is especially notable, as there are few materials that can electrocatalyze the conversion of CO<sub>2</sub> to CO in organic catholyte with even modest FEs.<sup>15</sup> Moreover, the few metals that drive this electrocatalytic process with reasonable current densities do so only upon application of very large overpotentials.16

Although Bi-CMEC with [BMIM]X ILs generates CO with FEs that are comparable to that observed with [EMIM], current densities for CO production ( $j_{CO}$ ) using the [BMIM] ILs were slightly higher than for the [EMIM] experiments (Table 1, Figure 2B) and are similar to those obtained using Ag or Au cathodes.<sup>12,15,17</sup> The Bi-CMEC system is robust under these conditions and displays steady current densities for CO production over several hours (Figure S4).

The energy efficiency of electrocatalytic CO production by Bi-CMEC can be calculated using Eq 2,

energy efficiency = 
$$\frac{FE \times E^{\circ}_{CO_2/CO}}{E}$$
 (2)

in which  $E^{\circ}_{CO_2/CO}$  represents the standard reduction potential for conversion of  $CO_2$  to CO under the CPE conditions and E is the applied potential.<sup>18</sup> Determination of the energy efficiency of the Bi-CMEC system requires an estimation of the standard potential of the CO<sub>2</sub>/CO redox couple ( $E^{\circ}_{CO_2/CO}$ ) and calculation of the overpotential  $(\eta)$  at which CPE is carried out. The position of  $E^{\circ}_{CO_{7}/CO}$  is dependent on the protondonating ability of the electrolyte solution.<sup>19</sup> For the present system, deprotonation of the central imidazolium carbon of the [EMIM] and [BMIM] ILs is the most likely source of protons to drive the  $2e^{-}/2H^{+}$  conversion of CO<sub>2</sub> to CO. The pK<sub>a</sub> value for deprotonation of these 1,3-dialkylimidazolium cations is approximately 32 in MeCN.<sup>20</sup> The low proton availability of the current system drives  $E^{\circ}_{CO_2/CO}$  to more negative potential, as this standard redox couple can be estimated to be -1.78 V on the basis of the  $pK_a$  values for deprotonation of [EMIM]

and [BMIM].<sup>21</sup> By contrast, the IL 1-butyl-2,3-dimethylimidazolium·BF<sub>4</sub> ([BMMIM]BF<sub>4</sub>), which bears a methyl substituent at the imidazolium 2-position, cannot be deprotonated as readily and does not induce CO<sub>2</sub> reduction catalysis with appreciable current density (Figure 2B, pink trace, Table 1) over the same potential range (Figure S3D). These results indicate that proton transfer from the imidazolium helps drive the observed CO<sub>2</sub> reduction chemistry and suggest that other organic acids may be able to promote a similar electrocatalysis.

Given that Bi-CMEC drives selective CO formation while operating with appreciable current density at E = -1.95 V, the overpotential for this process is only 0.165 V. This low overpotential coupled with the high FEs corresponds to an energy efficiency of over 85%. Both the low overpotential and high energy efficiency distinguish Bi-CMEC as a promising platform for electrocatalytic CO production, as both these values compare favorably to those obtained using Ag- and Aubased electrocatalysts, which are among the most efficient existing platforms for electrolytic generation of CO from CO<sub>2</sub>.<sup>12,15,17</sup>

The variation in partial current density of CO for Bi-CMEC on glassy carbon was measured as a function of applied overpotential in CO2-saturated MeCN containing 20 mM [BMIM]PF<sub>6</sub>. These data were obtained by performing steppedpotential electrolyses between E = -1.95 and -2.5 V, with commensurate quantification of the gaseous products by GC. The FE for CO production remains high as the applied  $\eta$  is increased; however, the resulting Tafel plot constructed from these data (Figure 2C) begins to deviate from linearity as the applied potential exceeds -2.1 V. This curvature may be due to uncompensated iR drop caused by the surface resistivity of the GCE. The Tafel data are linear in the range of  $\eta = 0.165 - 0.275$ V, with a slope of 139 mV/decade. This value, which is close to 118 mV/dec, points to a mechanistic pathway in which initial electron transfer to generate a surface-adsorbed CO2<sup>•-</sup> species is rate determining. This mechanism has been invoked for CO2 reduction at many heterogeneous electrodes.<sup>22</sup>

The electrocatalytic reduction of  $CO_2$  offers a promising route to the conversion of renewable sources of electric current to carbon-based fuels when coupled to the  $4e^-/4H^+$  splitting of water. A two-compartment cell for  $CO_2$  electrocatalysis allowed CO production at the Bi-CMEC-modified electrode to be coupled to water oxidation. In these experiments, the anode compartment consisted of a piece of platinum gauze in aqueous phosphate buffer (pH ~7.4), and the cathode compartment was comprised of the Bi-CMEC-modified GCE immersed in  $CO_2$ -saturated MeCN containing 0.1 M TBAPF<sub>6</sub> and 20 mM [BMIM]PF<sub>6</sub>. The two compartments were separated by a Nafion membrane. CV analysis of this split cell arrangement shows the same intense catalytic wave for  $CO_2$  reduction at approximately -1.9 V (Figure S5, inset) that was observed using the single-solvent arrangement.

CPE experiments using the split electrode/electrolyte arrangement showed initial current densities of approximately 9 mA/cm<sup>2</sup> with a FE of 52% for generation of CO (Figure S5). Together, these data correspond to a turnover frequency (TOF) of approximately 300 s<sup>-1</sup> for generation of CO, based on the electrochemical surface area of the Bi-CMEC electrode. Permeation of the Nafion membrane by water caused a gradual decrease in CO evolution activity to  $j_{tot} = 0.25$  mA/cm<sup>2</sup> with a FE of 39% for CO formation. This drop in FE for CO generation is due to enhanced production of HCO<sub>2</sub>H from CO<sub>2</sub> in the presence of an aqueous catholyte.<sup>9</sup> The Bi-CMEC

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assembly is robust under these conditions. Extended CPEs of over 12 h showed no additional decay in current density and produced over 85,000 cumulative surface turnovers over the course of the experiment, which is significantly higher than that obtained using a Ag cathode with an [EMIM]BF<sub>4</sub> cocatalyst.<sup>12</sup> It is expected that improved mass transport using a flow-cell, gas diffusion electrode, or other advanced cell design<sup>23,24</sup> would enable even higher current densities (TOFs) for CO production by Bi-CMEC. Additional improvements in activity may also be attained simply by improving ohmic contact between the Bi-CMEC and underlying GCE or by using an alternative substrate entirely.

Despite its low cost, Bi has been virtually ignored as a cathode material for CO2 electrolysis. As we have shown, however, electrodeposition of a material containing Bi<sup>0</sup> and Bi<sup>3+</sup> produces a catalyst that can efficiently drive CO generation in the presence of an IL. The activity of Bi-CMEC rivals that of the best noble-metal cathodes described to date, as this Bi<sup>0</sup>/Bi<sup>3+</sup> assembly catalyzes the conversion of CO<sub>2</sub> to CO with high selectivity and FE. At present, the importance of the Bi<sup>3+</sup> ions to the efficacy of Bi-CMEC is unclear. It is possible that the interface between Bi<sup>0</sup> and Bi<sup>3+</sup> sites serves to stabilize CO2. intermediates at the electrode surface in a fashion similar to that proposed for metal oxides on etched electrodes.<sup>25,26</sup> Alternatively, the exceptional activity of Bi-CMEC may be derived from in situ reduction of the Bi<sup>0</sup>/Bi<sup>3+</sup> material to generate metastable surfaces with enhanced catalytic properties. The use of imidazolium ILs may be especially critical in this regard,<sup>27</sup> as recent work has demonstrated that interplay between adsorbed imidazolium cations and CO2 at bulk platinum electrodes can significantly enhance electrocatalytic CO<sub>2</sub> reduction.<sup>28</sup> Future efforts to uncover the atomic-level structure of Bi-CMEC will be critical to understanding the mechanism by which this system activates CO2 and, more generally, may provide a rational route for the development of additional inexpensive electrode materials for CO evolution.<sup>29</sup>

#### ASSOCIATED CONTENT

#### **Supporting Information**

Experimental methods and electrochemistry data. This material is available free of charge via the Internet at http://pubs.acs.org.

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## Notes

The authors declare no competing financial interest.

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